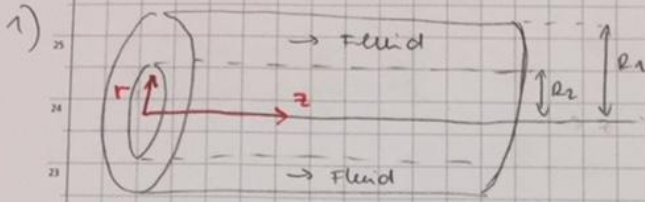


Homework 2



→ Renaming of coordinates!
 assumptions:
 - steady - laminar - incompressible flow
 - pressure-driven
 - flow along z-axis
 → using cylindrical coord. $(\frac{r}{z})$

a) $\vec{v} = [v_r(r, \theta, z), v_\theta(r, \theta, z), v_z(r, \theta, z)] \rightarrow v_z(r, z)$ irrotational flow
 $v_r = 0, v_\theta = 0$, along z-axis

mass conservation:
 (for incompressible flow)

$$\nabla \cdot \vec{v} = 0$$

$$\frac{1}{r} \frac{\partial}{\partial r} (r v_r) + \frac{1}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{\partial v_z}{\partial z} = 0$$

$v_r = 0, v_\theta = 0$

$$\textcircled{1} \rightarrow \frac{\partial v_z}{\partial z} = 0$$

→ v_z independent of z , $v_z(r)$

Navier-Stokes equation (only in z-direction as other 2 direction do not give any additional information → $v_r = v_\theta = 0$):

$$z: \rho \left(\frac{\partial v_z}{\partial t} + v_r \frac{\partial v_z}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_z}{\partial \theta} + v_z \frac{\partial v_z}{\partial z} \right) = -\frac{\partial p}{\partial z} + \mu \nabla^2 v_z + \rho b_z$$

steady $v_r = 0, v_\theta = 0$ mass cons. no body forces in z-dir.

$$\frac{\partial p}{\partial z} = \mu \left(\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2}{\partial \theta^2} (v_z) + \frac{\partial^2}{\partial z^2} (v_z) \right)$$

$v_z(r) \quad v_z(r)$

$\textcircled{2} \rightarrow \frac{\partial p}{\partial z} = \mu \left(\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) \right)$

$\textcircled{1}$ and $\textcircled{2}$ are the equations governing the flow

b) B.C: no-slip-condition at the walls: $v_z = 0$ at $r = R_2$
 $v_z = 0$ at $r = R_1$

c) $\textcircled{2}: \frac{r}{\mu} \frac{\partial p}{\partial z} = \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) \quad | \int dr$

$$B_1 + \frac{r^2}{2\mu} \frac{\partial p}{\partial z} = r \frac{\partial v_z}{\partial r}$$

$$B_1 + \frac{r}{2\mu} \frac{\partial p}{\partial z} = \frac{\partial}{\partial r} v_z \quad | \int dr \Rightarrow v_z(r) = \frac{\partial p}{\partial z} \frac{r^2}{4\mu} + B_1 \ln(r) + B_2$$

inserting BC. to get B_1, B_2 :

$$V(r=R_1) = 0$$

$$0 = \frac{\partial P}{\partial z} \frac{R_1^2}{4\mu} + B_1 \ln(R_1) + B_2$$

$$B_2 = -\frac{\partial P}{\partial z} \frac{R_1^2}{4\mu} - B_1 \ln(R_1)$$

$$B_2 = -\frac{\partial P}{\partial z} \frac{1}{4\mu} \left(\frac{\ln(R_1)(R_1^2 - R_2^2)}{\ln(R_2/R_1)} + R_1^2 \right)$$

$$\Rightarrow V_z(r) = \frac{\partial P}{\partial z} \frac{1}{4\mu} \left(r^2 - R_1^2 + \frac{(R_1^2 - R_2^2)}{\ln(R_2/R_1)} \cdot \ln\left(\frac{r}{R_1}\right) \right)$$

$$V(r=R_2) = 0$$

$$0 = \frac{\partial P}{\partial z} \frac{R_2^2}{4\mu} + B_1 \ln(R_2) + B_2$$

$$B_1 = \frac{\partial P}{\partial z} \frac{(R_1^2 - R_2^2)}{4\mu \ln(R_2/R_1)}$$

radius of maximum velocity:

$$\frac{dV_z}{dr} = \frac{\partial P}{\partial z} \frac{r}{2\mu} + \frac{B_1}{r} = \frac{\partial P}{\partial z} \frac{1}{2\mu} \left(r + \frac{(R_1^2 - R_2^2)}{2r \ln(R_2/R_1)} \right) \stackrel{!}{=} 0$$

$$r^* = \pm \sqrt{\frac{(R_2^2 - R_1^2)}{2 \ln(R_2/R_1)}}$$

maximum $\Rightarrow V_z''(r^*) < 0$

$$\Rightarrow \frac{\partial P}{\partial z} < 0$$

\rightarrow 2 radii of max. velocity as flow is symmetric

d) volume flow rate: $Q = A \cdot v = \int_0^{2\pi} \int_{R_2}^{R_1} V_z(r) r dr d\theta$

$$= 2\pi \int_{R_2}^{R_1} \left(\frac{\partial P}{\partial z} \frac{r^3}{4\mu} + B_1 \ln(r) \cdot r + B_2 \cdot r \right) dr$$

$$(*) : \int_{R_2}^{R_1} \ln(r) \cdot r dr = \left[r(r \ln(r) - r) \right]_{R_2}^{R_1} - \int_{R_2}^{R_1} r \ln(r) - r dr$$

$$2 \cdot \int_{R_2}^{R_1} \ln(r) \cdot r dr = \left[r^2 (\ln(r) - 1) \right]_{R_2}^{R_1} - \int_{R_2}^{R_1} r dr$$

$$\int_{R_2}^{R_1} \ln(r) \cdot r dr = \frac{1}{2} \left[r^2 (\ln(r) - 1) \right]_{R_2}^{R_1} - \frac{1}{4} \left[r^2 \right]_{R_2}^{R_1}$$

$$Q = 2\pi \cdot \frac{\partial P}{\partial z} \frac{1}{2\mu} \left[\frac{R_1^4}{4} - \frac{R_2^4}{4} - \left(\frac{\ln(R_1)(R_1^2 - R_2^2)}{\ln(R_2/R_1)} + R_1^2 \right) \frac{(R_1^2 - R_2^2)}{2} \right]$$

$$+ \frac{(R_1^2 - R_2^2)}{\ln(R_2/R_1)} \left(\frac{R_1^2}{2} (\ln(R_1) - \frac{1}{2}) - \frac{R_2^2}{2} (\ln(R_2) - \frac{1}{2}) \right)$$

$$= \frac{\partial P}{\partial z} \frac{\pi}{2\mu} \left[\frac{R_1^4}{4} - \frac{\phi^4 R_1^4}{4} + \frac{\phi^2 R_1^2 \ln(R_1) - R_1^2 \ln(\phi R_1)}{2 \ln(\phi)} (R_1^2 - \phi^2 R_1^2) \right]$$

$$+ \frac{(R_1^2 - \phi^2 R_1^2)}{2 \ln(\phi)} \left(R_1^2 (\ln(R_1) - \frac{1}{2}) - \phi^2 R_1^2 (\ln(\phi R_1) - \frac{1}{2}) \right)$$

$$\phi = \frac{R_2}{R_1}$$

$$R_2 = \phi R_1$$

e)

$$\lim_{\phi \rightarrow 0} \frac{\partial p}{\partial z} \frac{\pi}{2\mu} \left[\frac{R_1^4}{4} - \frac{\phi^4 R_1^4}{4} + \frac{\phi^2 R_1^2 \ln(R_1) - R_1^2 \ln(\phi R_1)}{2 \ln(\phi)} (R_1^2 - \phi^2 R_1^2) \right]$$

$$+ \frac{(R_1^2 - \phi^2 R_1^2)}{2 \ln(\phi)} \left(R_1^2 \left(\ln(R_1) - \frac{1}{2} \right) - \phi^2 R_1^2 \left(\ln(\phi R_1) - \frac{1}{2} \right) \right)$$

single terms:

$$\lim_{\phi \rightarrow 0} \frac{\phi^2 R_1^4 \ln(R_1)}{2 \ln(\phi)} \xrightarrow{\Delta \infty} \lim_{\phi \rightarrow 0} \frac{2\phi R_1^4 \ln(R_1)}{2 \frac{1}{\phi}} = 0 \rightarrow \text{same for terms multiplying } (-\phi^2 R_1^2)$$

$$\lim_{\phi \rightarrow 0} \frac{-R_1^4 \ln(\phi R_1)}{2 \ln(\phi)} = \lim_{\phi \rightarrow 0} \frac{-R_1^4 \ln(\phi)}{2 \ln(\phi)} - \frac{R_1^4 \ln(R_1)}{2 \ln(\phi)} \rightarrow -\infty$$

$$= -\frac{R_1^4}{2}$$

↳ using de l'Hopital as previously, one can see that all the terms from above tend to 0 as $\phi \rightarrow 0$ other

all in all:

$$\lim_{\phi \rightarrow 0} (Q) = \frac{\partial p}{\partial z} \frac{\pi}{2\mu} \left[\frac{R_1^4}{4} - \frac{R_1^4}{2} \right] = -\frac{\partial p}{\partial z} \frac{\pi}{2\mu} \frac{R_1^4}{4}$$

for $R_1 = \frac{D}{2}$:

$$\lim_{\phi \rightarrow 0} (Q) = -\frac{\partial p}{\partial z} \frac{\pi D^4}{128\mu}$$

↳ this is the formula of volume flow rate for circular Poiseuille flow.

$\phi \rightarrow 0 \Rightarrow R_1 \gg R_2 \rightarrow$ in this case we have a flow in a cylindrical tube instead of a flow in the annular space of two coaxial tubes

↳ usual Poiseuille case.



2) boundary layer $\delta(x)$

$$\frac{u}{U} = a + b \frac{y}{\delta} + c \left(\frac{y}{\delta}\right)^2 \quad \text{with} \quad u=0 \quad \text{at} \quad y=0$$

$$u=U, \quad \frac{\partial u}{\partial y} = 0 \quad \text{at} \quad y=\delta$$

$$a=0$$

$$1 = b + c \quad \frac{\partial u}{\partial y} = \frac{U b}{\delta} + \frac{2 y c U}{\delta^2} \rightarrow -2c = b \rightarrow b = -2c$$

$$1 = -2c + c \rightarrow c = -1, \quad b = 2$$

$$\rightarrow \frac{u}{U} = 2 \frac{y}{\delta} - \left(\frac{y}{\delta}\right)^2$$

Kármán-Pohlhausen: drag force on a flat plate with momentum thickness θ :

$$D(x) = \rho b U^2 \theta$$

for uniform flow
b... thickness plate

$$\text{and} \quad \theta = \int_0^\delta \frac{u}{U} \left(1 - \frac{u}{U}\right) dy$$

$$\rightarrow \frac{dD(x)}{dx} = \rho b U^2 \frac{d\theta}{dx}$$

drag force $\hat{=}$ integrated shear stress along the plate:

$$D(x) = b \int_0^x \tau_w(x) dx \rightarrow \frac{dD(x)}{dx} = b \tau_w(x)$$

momentum-integral relation

for flat plate boundary layer:

$$\tau_w(x) = \rho U^2 \frac{d\theta}{dx}$$

$$\text{here: } \theta = \int_0^\delta \left(2 \frac{y}{\delta} - \left(\frac{y}{\delta}\right)^2\right) \left(1 - 2 \frac{y}{\delta} + \left(\frac{y}{\delta}\right)^2\right) dy$$

$$= \int_0^\delta \left(2 \frac{y}{\delta} - 5 \frac{y^2}{\delta^2} + 4 \frac{y^3}{\delta^3} - \frac{y^4}{\delta^4}\right) dy$$

$$= \left[\frac{y^2}{\delta} - \frac{5}{3} \frac{y^3}{\delta^2} + \frac{y^4}{\delta^3} - \frac{1}{5} \frac{y^5}{\delta^4} \right]_0^\delta = \frac{2}{15} \delta \rightarrow \frac{d\theta}{dx} = \frac{2}{15} \frac{d\delta}{dx}$$

$$\tau_w = \mu \frac{\partial u}{\partial y} \Big|_{y=0} = \mu \left(\frac{2U}{\delta} - \frac{2Uy}{\delta^2} \right) \Big|_{y=0} = \frac{2U\mu}{\delta}$$

$$\rightarrow \tau_w = \rho U^2 \frac{d\theta}{dx}$$

$$\frac{2U\mu}{\delta} = \rho U^2 \frac{2}{15} \frac{d\delta}{dx}$$

$$\int \frac{15}{U} \frac{\mu}{\rho} dx = \int \delta d\delta$$

with $\delta(x)=0$
at $x=0$

$$\frac{15}{U} \nu x = \frac{1}{2} \delta^2$$

$$\delta = \sqrt{\frac{30 \nu x}{U}} \quad | \cdot \frac{1}{x}$$

$$\frac{\delta}{x} = 5.477 \cdot \text{Re}_x^{-1/2}$$

$$\approx \frac{5.0}{\text{Re}_x^{1/2}} \quad \text{Blasius}$$

\rightarrow our solution
is a good
approximation
to Blasius'
exact solution.